



Engineering perspective of electrochlorination system for ballast water treatment using carbon dioxide

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Abstract: Electrochlorination systems are widely used in ballast water treatment because they are more cost-effective than other disinfection techniques. Furthermore, the on-board generation of hypochlorous acid from electrochlorination systems has advantages in terms of footprint size and safety as there is no need to store highly concentrated hypochlorite solutions. Recently, several studies focused on the injection of carbon dioxide into an electrochlorination system to enhance disinfection efficacy. However, the treatment efficacy of injecting exhaust gas into an electrochlorination system remains understudied. In this study, the disinfection efficacy of *Artemia* sp. was investigated based on the holding time when carbon dioxide was injected into the electrochlorination system. Disinfection efficacy significantly improved as the pH decreased to 5.5. Additionally, the pH inside the ballast water tank adjusted based on ballast water flow capacity when the carbon dioxide from combustion engine was fully dissolved. Our results showed that the pH suitable for eliminating microorganisms was achieved using only the auxiliary engine without any acid additives. This study provides a promising conceptual design for ballast water treatment.

Keywords: Ballast water treatment, Electrochlorination system, Disinfection efficacy, Exhaust gas, Carbon dioxide

1. Introduction

Ballast water is transferred by vessels to ensure stability during voyages. Ballasting and deballasting operations are performed to offset changes in vessel displacements associated with unloading and loading, respectively. However, the various biological substances contained in ballast water can affect native species and cause ecological changes in the ocean [1].

To prevent invasive species from translocating via ballast water, ballast water should be treated and disinfected in accordance with the United States Coast Guard (USCG) and International Maritime Organization (IMO) regulations. In 2019, the IMO announced a list of approved ballast water treatment systems (BWTS) in accordance with the procedure. The 45 BWTS consists mainly of filtration, electrolysis, UV, ozone treatment, and chemical injection systems [2]-[3]. Among the BWTS, electrochlorination is preferred because it provides relatively low power consumption, cost, footprint area, and higher disinfection efficacy [3].

To enhance the removal of marine organisms, Cha *et al.* [4]

examined the synergistic effects of carbon dioxide (CO₂) injection on electrochlorination disinfection of *Artemia franciscana*. It is well known that injected CO₂ can be converted into carbonic acid (H₂CO₃^{*}) in water, leading to a decrease in the pH of water. At low pH, hypochlorous acid (HOCl) is formed more than the less powerful oxidative hypochlorite (OCl⁻). HOCl is 80-200 times stronger than OCl⁻ in terms of pathogen disinfection [4]. In general, exhaust gas is a mixture of gases and contains mainly CO₂, NO_x, and SO₂. Under these circumstances, CO₂ generated from combustion engines can be a valuable source for the elimination of microorganisms (*e.g.*, zooplankton and phytoplankton) because the exhaust gas can minimize energy consumption instead of the CO₂ gas generation system. However, there are insufficient documents on the composition and treatment efficacy of exhaust gas in ballast water treatment to draw clear conclusions [5].

In this study, we focused on the influence of treatment efficacy by utilizing exhaust gas as a CO₂ source and proposed a promising conceptual design for a new type of BWTS.

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2. Experimental

2.1 Preparation of Test Water

The test water (100 L) was salinated (salinity > 32 PSU) using a mixture of dissolved mineral salts (Reef Salt, Aquaforest, Poland). The composition of the mixture was as follows: 19,000–19,500 mg/L chlorine, 9,700–11,800 mg/L sodium, 1,300–1,360 mg/L magnesium, 810–990 mg/L sulfur, 410–430 mg/L calcium, and 360–380 mg/L potassium.

2.2 Microorganism Preparation and Enumeration

To meet the required test conditions stipulated in the IMO G8 guidelines, 10^5 individuals/ m^3 for organisms of size $\geq 50 \mu m$ representing zooplankton, *Artemia* sp., which is relatively easy to culture and assay, was hatched from the dehydrated cysts. The temperature of the test water was maintained at 26°C for 2–3 days to provide oxygen during cyst development. *Artemia* sp. was enumerated using an optical microscope (Olympus SZ51). First, *Artemia* sp. was passed through 50 μm a homemade mesh sieve. The volume of the concentrated sample was 50 mL and approximately 1 mL was taken using an EppendorfTM micropipette. An appropriate amount of test water that did not contain living organisms was added so that light could pass through the Bogorov counting chamber well. During the visual inspection, the immobile *Artemia* sp. was checked by moving the needle to confirm whether the organism was alive.

2.3 Electrochlorination and CO₂ Injection System

A laboratory-scale electrochlorination system was set up, and the same electrode as the HiBallastTM BWTS (IMO & USCG Type Approval Certificate) was used. The electrical current was controlled to adjust the total residual oxidant (TRO) concentration to 4 ppm using the same electrode. Afterward, CO₂ (99.9%, KNG Co., Ltd.) was injected at a flow rate of 100–300 ml/min to lower the pH of the test water. For more detailed information, please refer to the schematic of the water treatment apparatus (see **Figure S1**).

2.4 Water Quality Parameter Measurements

The pH of the test water was measured using a pH meter (HM-40P; TOADKK, Japan). Dissolved oxygen (DO) concentration was measured using a DO meter (DO-31P; TOADKK, Japan), and the concentrations of chlorine (mg/L as Cl₂) were determined using *N,N*-diethyl-*p*-phenylenediamine (DPD; Hach Company, USA) using a colorimetric method (See **Figure S1**).

3. Results and Discussion

Figure 1 shows the inactivation of *Artemia* sp. at different pH values in the presence of 4ppm TRO concentration. CO₂ was used to adjust the pH of test water. When the pH was lowered from 8.2 to 5.5, the inactivation of *Artemia* sp. increased by approximately 3, 7, and 29 times on days 1, 2, and 3 of holding time, respectively. This agrees well with previous results that CO₂ injection strengthens disinfection efficacy against microorganisms compared to the electrochlorination system alone [4][6]. According to earlier studies, the efficacy of electrochlorination relies heavily on HOCl concentration in water. Previous studies also explained that reduced pH increases the HOCl concentration in the solution, and the disinfection efficacy of HOCl is much higher than that of ClO⁻ (considering that the pKa of HOCl is 7.53) [4][6]. Meanwhile, estimates showed that the disinfection efficacy greatly increased as the decomposition reaction of foreign substances accelerated and biological toxins increased on day 3.

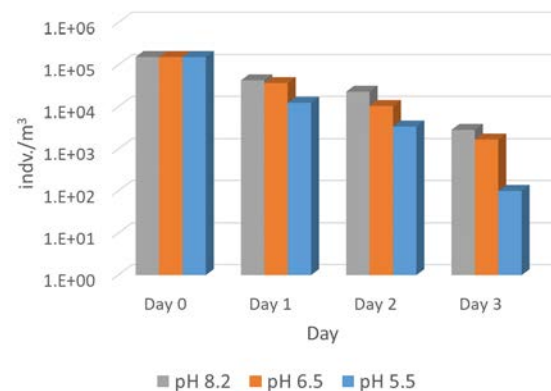


Figure 1: Inactivation of *Artemia* sp. with respect to different pH. The initial TRO concentration was 4 ppm and pH was controlled by CO₂ injection

Figure 2 shows dissolved oxygen (DO) concentration as a function of pH. Overall, the DO concentration steadily decreased with increasing holding time and constantly decreased with decreasing pH, indicating that disinfection efficacy is related to DO concentration. There was no significant change in the concentration between 1 and 3 days of holding time at pH 5.5, implying that the enhanced inactivation of *Artemia* sp. on day 3 was not directly correlated with changes in DO concentration. Although TRO concentration decay was more noticeable in only electrochlorinated water than in electrochlorinated water with CO₂ addition [4]. Our results did not show a drastic difference in the

TRO concentration decay profiles (data not shown here). Further studies are needed to elucidate the cause of the enhanced disinfection efficacy.

It is worthwhile to review the technique that was most effective for disinfection. As shown in **Figure 3**, the inactivation efficacy of *Artemia* sp. was 98.8%, 99.4%, and 99.9% in CO₂ alone, 4 ppm TRO, and 4 ppm TRO + CO₂ on day 3 of the holding time, respectively. From an engineering perspective, CO₂ can be constantly injected to maintain a certain level of disinfection in ballast water tanks, and electrochlorination systems with CO₂ addition can be used when entering the United States, where USCG ballast water treatment regulations are applied. Accordingly, it would be helpful to reduce the power consumption of BWTS.

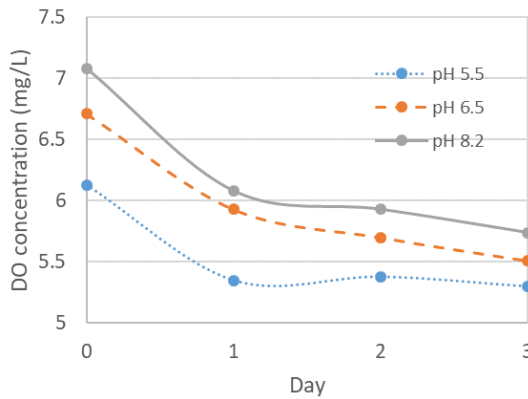


Figure 2: Dissolved oxygen (DO) concentration according to pH change

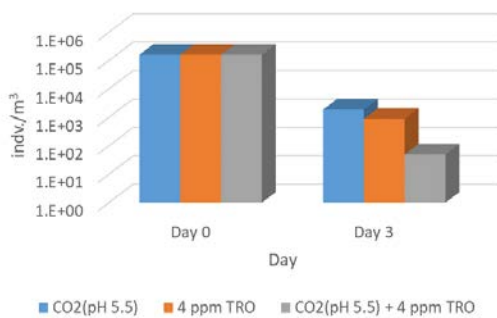


Figure 3: Comparison of *Artemia* sp. individuals: CO₂, 4 ppm TRO, and CO₂ + 4ppm TRO injection

Some BWTS manufacturers have attempted to use CO₂ gas generation systems as the CO₂ source. To our knowledge, there are no cases of direct application to BWTS using vessel exhaust gas. Therefore, it is important to verify if the exhaust gas emitted

from a combustion engine can be applied to a BWTS. **Table 1** shows the summary of auxiliary engine exhaust monitored. Maximum continuous rating (MCR) was 1,540 kW at a 75% engine load, and the exhaust gas flow rate was 7,066 kg/h. In addition, the CO₂ concentration was approximately 5.62%.

Table 1: Summary of auxiliary engine exhaust monitored

Engine power	Engine load	Exhaust gas flow rate	CO ₂ conc.	NOx conc.	SOx conc.
1,540 kW	75%	7,066 kg/h	5.62%	218 ppm	Negligible

When injected CO₂ is dissolved in water, the concentrations of [H₂CO₃^{*}], [HCO₃⁻], and [CO₃²⁻] can be predicted using Equations (1)–(3). The total inorganic carbon (C_T) is expressed by Equation (4), which is the sum of [H₂CO₃^{*}], [HCO₃⁻], and [CO₃²⁻].

$$[H_2CO_3^*] = C_T / (1 + KHCO_3^- \cdot 1/[H^+] + KHCO_3^- \cdot KCO_3^{2-} \cdot 1/[H^+]^2) \tag{1}$$

$$[HCO_3^-] = KHCO_3^- \cdot [H_2CO_3^*] / [H^+] \tag{2}$$

$$[CO_3^{2-}] = KCO_3^{2-} \cdot [H_2CO_3^*] / [H^+]^2 \tag{3}$$

$$C_T = \dot{m}_{CO_2} \text{ (kg/s)} / 44 \text{ (g/mol)} / \text{Flow capacity (L/s)} \\ = [H_2CO_3^*] + [HCO_3^-] + [CO_3^{2-}] \tag{4}$$

The equilibrium constants for KHCO₃⁻ and KCO₃²⁻ were analytically obtained using **Equation (5)** [7].

$$\log K = a_1 + a_2/T + a_3T + a_4 \log T + a_5/T^2 \tag{5}$$

where T is the absolute temperature, and a₁ to a₅ are empirical constants.

To calculate the pH inside the ballast water tank, the concentration of H⁺ was determined using *Excel* software. The dissolved inorganic carbon (DIC) concentration in the ballast water tank as a function of flow capacity is shown in **Figure S2**.

Table 2 shows the predicted pH inside the ballast water tank as a function of ballast water flow capacity. The ballast water flow capacity will be approximately 500 m³/h when the pH is 5.5, and it is indicated as the highest disinfection efficacy. A pH was predicted to be 5.9 when the ballast water flow capacity reached 1000 m³/h, that is, under conditions where vessels are frequently operated. From these results, a suitable pH for microorganism disinfection was achieved using only the vessel auxiliary engine

without any acid additives.

Table 2: Predicted pH in ballast water tank as a function of ballast water flow capacity. Exhaust gas ratio was fixed to 50%, and the ballast water temperature was 22°C

Ballast water flow capacity	pH in ballast water tank
500 m ³ /h	5.59
1,000 m ³ /h	5.96
2,000 m ³ /h	6.48
3,000 m ³ /h	7.12

Finally, the IMO calls for the maritime industry to restrict its CO₂ emissions by -40% by 2030 and -70% by 2050, compared to the base level in 2008 [8]. In view of the upcoming CO₂ emission regulations, many shipbuilding manufacturers have begun researching the possibility of onboard carbon capture vessels. They have mainly focused on CO₂ capture and storage using chemical absorbents. However, it will be difficult to apply to vessels owing to corrosion caused by chemical adsorbents and the expensive operation cost required to regenerate the chemical absorbent. However, if the injected CO₂ in the ballast water tank is periodically neutralized during the voyage and discharged after attaining a pH similar to that of seawater, it is expected that CO₂ can be partially reduced [9]. The proposed concept of an electrochlorination system combined with CO₂ injection is illustrated in

Figure 4.

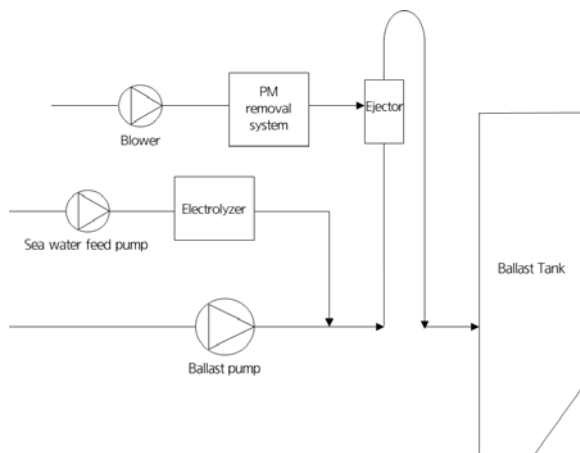


Figure 4: Schematic of electrochlorination system combined with CO₂ injection

4. Conclusions

We investigated the inactivation of *Artemia* sp. using an electrochlorination system combined with CO₂ injection. At pH 5.5, the inactivation of *Artemia* sp. significantly increased by approximately 29 times compared to pH 8.4 on day 3 of holding time.

Results showed that the main factors enhancing the disinfection efficacy were an increase in HOCl concentration with decreasing pH and a decrease in DO concentration due to the dissolution of CO₂. Results of comparing disinfection efficacies revealed that the inactivation of *Artemia* sp. was 98.8%, 99.4%, and 99.9% in CO₂ alone, 4 ppm TRO, and 4 ppm TRO + CO₂ on day 3 of the holding time, respectively.

From an engineering perspective, it can be concluded that the CO₂ emitted from a combustion engine can be directly used to reduce pH. Furthermore, if the injected CO₂ in ballast water tanks is periodically neutralized during the voyage and discharged after attaining a pH similar to that of seawater, it is expected that CO₂ can be partially eliminated. We hope that this study will provide insight into how to retrofit and design BWTS in the maritime industry.

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Author Contributions

Conceptualization, J. Joo; Investigation, D. H. Park; Data Curation, D. H. Park; Writing-Original Draft Preparation, J. Joo; Writing-Review & Editing, T-J. Rhee and J. H. Lee.

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